

Corrections

Application of a Multicomponent Thermodynamic Model to Activities and Thermal Properties of 0–40 mol kg⁻¹ Aqueous Sulfuric Acid from <200 to 328 K. Simon L. Clegg and Peter Brimblecombe, *J. Chem. Eng. Data* **1995**, 40, 43–64.

Our attention has recently been drawn¹ to typographical errors in two equations in the above paper.

Page 44. The final term in eq 9 ($0.75E_{\text{SO}_4}W_{1,\text{H-SO}_4}$) should be preceded by a minus sign, not a plus as given in the paper. A similar error is present in eq 10, and the final term in that expression ($2E_{\text{HSO}_4}W_{1,\text{H-HSO}_4}$) should also be preceded by a minus sign.

Both typographical errors were not present in the computer programs used to fit the thermodynamic model, thus the results and parameter values presented are unchanged.

(1) Zaveri, R. Personal communication, Department of Chemical Engineering, Virginia Polytechnic Institute, Blacksburg, VA.

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Vapor–Liquid Equilibria for the Systems Composed of 1-Chloro-1,1-difluoroethane, 1,1-Dichloro-1-fluoroethane, and 1,1-Trichloroethane at 50.1 °C. Yun Whan Kang and Youn Yong Lee, *J. Chem. Eng. Data* **1996**, 41, 303–305.

The correct version of Table 2 follows.

Table 2. Vapor–Liquid Equilibrium Data for HCFC-142b (1) + HCFC-141b (2) + HCC-140a (3) at 50.1 °C

<i>P</i> /kPa	<i>x</i> ₁	<i>x</i> ₂	<i>y</i> ₁	<i>y</i> ₂
93.4	0.1571	0.2083	0.6240	0.2131
211.9	0.1628	0.3355	0.5737	0.3075
231.6	0.1644	0.5012	0.5101	0.4161
255.0	0.1648	0.6690	0.4592	0.5063
302.4	0.3293	0.1670	0.8067	0.1070
318.7	0.3296	0.3347	0.7380	0.2036
335.8	0.3305	0.5019	0.6771	0.2956
404.5	0.4985	0.1671	0.8682	0.0848
418.2	0.5011	0.3329	0.8137	0.1622
195.0	0.1646	0.1662	0.6717	0.1637
265.3	0.2403	0.3660	0.6570	0.2681
500.0	0.6674	0.1664	0.9084	0.0712

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